

OPTIMIZATION OF MICROWAVE HYDRODISTILLATION OF DRIED PATCHOULI LEAVES BY RESPONSE SURFACE METHODOLOGY

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ABSTRACT

This paper deals with the optimization of patchouli oil yield in microwave hydrodistillation using response surface methodology (RSM). The factors considered were microwave power (A), feed to the solvent ratio (B) and extraction time (C). These parameters were varied at two levels. The conditions of optimum patchouli oil yield predicted were microwave power of 467.517 W, feed to solvent ratio of 0.432 g/mL and extraction time of 152.122 min. These factors gave an optimum patchouli oil yield of 4.862%. The significant model terms are extraction time. Analysis of variance (ANOVA) indicates that the model was significant as evidenced from R^2 of 0.9036 and the model F-value of 7.29. The patchouli oil yield predicted by the model was closed to the experimentally determined values (1.85 % and 1.87 % respectively); hence the model can be used for prediction of patchouli oil yield in essential oil extraction from dried patchouli leaves using microwave hydrodistillation method.

Keywords: Box-Behnken design; microwave hydrodistillation; patchouli oil.

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INTRODUCTION

Patchouli is one of the essential oil producing plants which is quite important as Indonesia's export commodity and contributes about 60% of the total export of Indonesian essential oil. Indonesia is the world's largest supplier of patchouli oil with the contribution of 90%¹. Currently, the extraction of patchouli oil is still done using conventional methods that generally have a smaller yield, takes relatively long time and requires a large cost. This is supported by research data that the extraction of basil oil using hydrodistillation method with feed to solvent ratio of 0.5 g/mL for 1 hour obtained yield as much as $0.95 \pm 0.08\%$ (v/w)². Therefore, consideration should be given to using a new "green technique" in the extraction of essential oils with minimum energy, solvent, and time usage. Until now it has developed new methods to extract essential oils, one of which is using the microwave (microwave-assisted extraction).

Previous research has shown that the extraction using the microwave is an alternative that could be developed than the conventional methods, because of the high levels of product purity, lack of solvent usage, and processing time is short³. Some extraction using the microwave that has been successfully developed is microwave hydrodistillation method which is a combination of hydrodistillation with microwave heating⁴.

This is supported by previous studies that had been conducted by Asghari et al.⁵ which showed that the extraction of essential oil from *Ferulago angulata* using microwave hydrodistillation method is more effective and efficient when compared with hydrodistillation method. Based on these research, the extraction of essential oil from *Ferulago angulata* using microwave hydrodistillation method with feed to solvent ratio of 0.067 g/mL and microwave power of 650 W for 70 minutes obtained a yield of 3.8%. While for the extraction of essential oil from *Ferulago angulata* using hydrodistillation method with feed to solvent ratio of 0.083 g/mL for 3 hours obtained a yield of 1.7%⁵. Therefore, in this study conducted extraction of patchouli oil using microwave hydrodistillation method.

In the extraction of patchouli oil using microwave hydrodistillation, the extraction parameters need to be optimized. Response Surface Methodology (RSM) is a collection of mathematical and statistical techniques useful for modeling and analyzing of problems in which a response of interest is influenced by some quantitative variables with the objective of optimizing the response⁶. In this study, an attempt was made at optimizing microwave hydrodistillation of patchouli oil using response surface methodology.

EXPERIMENTAL

Material and Chemicals

The dried patchouli leaves used in this study were obtained from Trenggalek, East Java, Indonesia and have a size of 2.45 ± 0.56 cm. The distilled water and anhydrous sodium sulfate used in the study were of analytical grade.

Microwave Hydrodistillation Method

In employing microwave hydrodistillation, we used a domestic microwave oven (EMM2308X, Electrolux, maximum delivered power of 800 W) with a wave frequency of 2450 MHz. The dimensions of the PTFE-coated cavity of the microwave oven were 48.5 cm x 37.0 cm x 29.25 cm. The microwave oven was modified by drilling a hole at the top. A round bottom flask with a capacity of 1000 ml was placed inside the oven and was connected to the three-way adapter and liebig condenser through the hole. Then, the hole was closed with PTFE to prevent any loss of the heat inside.

Some feed to solvent ratio (0.3; 0.4; 0.5 g/mL) were placed in the reaction flask and heated by microwave irradiation with various power (300; 450; 600 W) and various extraction time (60; 120; 180 min). The different densities and their immiscibility required that the water and patchouli oil be separated from each other by separating funnel and the excess water be refluxed to the extraction vessel in order to provide uniform conditions of solid-to-liquid ratios for extraction. The patchouli oil was collected in amber vials, dried under anhydrous sodium sulfate and stored at 4°C. The extraction yield of patchouli oil was calculated according to the equation given:

$$\text{Extraction yield (\%, w/w)} = \frac{\text{Mass of extracted patchouli oil}}{\text{Mass of dried patchouli leaves} \times (1 - \text{water content})} \times 100 \quad (1)$$

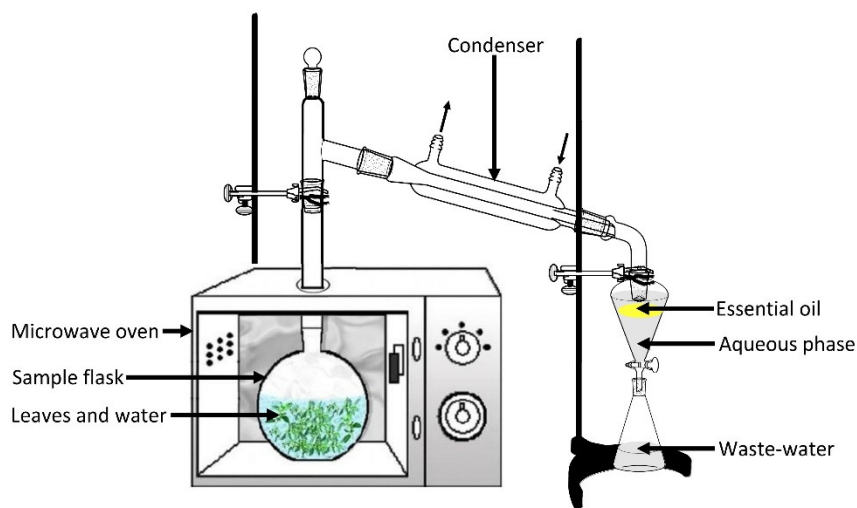


Fig.-1: Schematic representation of the microwave hydrodistillation apparatus used in this study

Design of Experiment

A 2^3 Box-Behnken Design (BBD) was employed resulting in a total of 17 experiments using the Design-Expert version 9.0.4.1 (State-Ease Inc., Minneapolis, MN, USA) to optimize the chosen key factors namely microwave power (A), feed to the solvent ratio (B) and extraction time (C). These variables each at two levels, low and high: A (300 – 600 W), B (0.3 – 0.5 g/mL) and C (60 – 180 min) are presented in Table-1.

These levels were chosen based on the capacity of the experimental set up for variables A and B, while C was selected based on experimental run time. The experimental design is shown in Table-2.

Table-1: Design summary

| Factors | Name | Units | Low Actual | High Actual | Low Coded | High Coded |
|---------|-----------------------|-------|------------|-------------|-----------|------------|
| A | Microwave power | W | 300 | 600 | -1 | 1 |
| B | Feed to solvent ratio | g/mL | 0.3 | 0.5 | -1 | 1 |
| C | Extraction time | min | 60 | 180 | -1 | 1 |

The regression analysis was performed to estimate the response function as a second order polynomial

$$Y = \beta_0 + \sum_{i=1}^k \beta_{ii} X_i^2 + \sum_{i=1}^{k-1} \sum_{j=2}^k \beta_{ij} X_i X_j \quad (2)$$

where Y is the predicted response, X_i is the uncoded value of the i -th test variable, β_0 , β_j and β_{ij} are coefficients estimated from the regression according to Rajasimman et al.⁷

A statistical program package Design-Expert version 9.0.4.1 (State-Ease Inc., Minneapolis, MN, USA) was used for regression analysis of the data and for estimating the coefficient of the regression equation. The equations were validated by the analysis of variance (ANOVA) test. Model and regression coefficients were considered significant when the p-value was lower than 0.05⁸.

Table-2: Box-Behnken Design matrix

| Run | Actual variables | | | Yield (%) | | |
|-----|------------------|----------|---------|--------------|-----------|---------|
| | A (W) | B (g/mL) | C (min) | Experimental | Predicted | Residue |
| 1 | 300 | 0.3 | 120 | 3.0221 | 2.7454 | 0.2767 |
| 2 | 300 | 0.4 | 60 | 2.3617 | 2.2383 | 0.1234 |
| 3 | 300 | 0.4 | 180 | 3.7482 | 3.7070 | 0.0412 |
| 4 | 300 | 0.5 | 120 | 2.7831 | 3.2250 | -0.4419 |
| 5 | 450 | 0.3 | 60 | 2.4343 | 2.8349 | -0.4006 |
| 6 | 450 | 0.3 | 180 | 3.3429 | 3.6613 | -0.3185 |
| 7 | 450 | 0.4 | 120 | 4.6493 | 4.6495 | -0.0002 |
| 8 | 450 | 0.4 | 120 | 4.6493 | 4.6495 | -0.0002 |
| 9 | 450 | 0.4 | 120 | 4.6493 | 4.6495 | -0.0002 |
| 10 | 450 | 0.4 | 120 | 4.6493 | 4.6495 | -0.0002 |
| 11 | 450 | 0.4 | 120 | 4.6493 | 4.6495 | -0.0002 |
| 12 | 450 | 0.5 | 60 | 3.3471 | 3.0291 | 0.3180 |
| 13 | 450 | 0.5 | 180 | 4.9240 | 4.5239 | 0.4001 |
| 14 | 600 | 0.3 | 120 | 3.6771 | 3.2356 | 0.4415 |
| 15 | 600 | 0.4 | 60 | 3.0438 | 3.0855 | -0.0416 |
| 16 | 600 | 0.4 | 180 | 3.8141 | 3.9379 | -0.1238 |
| 17 | 600 | 0.5 | 120 | 3.5357 | 3.8128 | -0.2771 |

RESULTS AND DISCUSSION

Table-2 presents the Box-Behnken Design matrix and the patchouli oil yield obtained for each experimental run. Analysis of variance for the response surface model is presented in Table-3. The analysis indicates that the model F-value of 7.29 implies the model is significant. There is only a 0.79% chance that an F-value this large could occur due to noise, the model also has a satisfactory level of adequacy (R^2). In this study C, A^2 , B^2 and C^2 are significant model terms ($p < 0.05$).

Table-3: Analysis of variance (ANOVA) for response surface quadratic model to identify significant factors affecting the patchouli oil yield

| Source | Sum of Squares | df | Mean Square | F Value | p-Value |
|--------|----------------|----|-------------|---------|---------|
| Model | 10.31 | 9 | 1.15 | 7.29 | 0.0079* |
| A | 0.58 | 1 | 0.58 | 3.69 | 0.0960 |
| B | 0.56 | 1 | 0.56 | 3.55 | 0.1015 |

| | | | | | |
|----------------|----------|----|----------|-------|---------|
| C | 2.69 | 1 | 2.69 | 17.13 | 0.0044* |
| AB | 0.002385 | 1 | 0.002385 | 0.015 | 0.9054 |
| AC | 0.095 | 1 | 0.095 | 0.60 | 0.4625 |
| BC | 0.11 | 1 | 0.11 | 0.71 | 0.4272 |
| A ² | 2.92 | 1 | 2.92 | 18.56 | 0.0035* |
| B ² | 1.33 | 1 | 1.33 | 8.47 | 0.0227* |
| C ² | 1.39 | 1 | 1.39 | 8.85 | 0.0207* |
| Residual | 1.10 | 7 | 0.16 | | |
| Lack of Fit | 1.10 | 3 | 0.37 | | |
| Pure Error | 0.000 | 4 | 0.000 | | |
| Cor Total | 11.41 | 16 | | | |

Standard deviation: 0.40; R²: 0.9036; Adj R²: 0.7796; Pred R²: -0.5427; Adeq precision: 7.928

*Significant variable

The Pred R² of -0.5427 implies that the overall mean is a better predictor of the response than the current model. Adeq Precision measures the signal to noise ratio; the ratio of 7.928 obtained indicates an adequate signal (a ratio greater than 4 is desirable). Therefore the model can be used to navigate the design space.

The response surface curves are plotted to understand the interaction of the variables and the optimum level of each variable for maximum response⁷. The response surface curves for extraction of patchouli oil using microwave hydrodistillation are presented in Fig.-2. Fig.-2(a) shows the interaction of microwave power and feed to solvent ratio on the yield, while Fig.-2(b) and 2(c) indicates interaction of microwave power and extraction time on the yield as well as that of feed to solvent ratio and extraction time on the yield, respectively. Final equation in terms of actual variables is given by Equation-3.

$$\begin{aligned} \text{Yield} = & -16.46046 + 0.036499 A + 43.55528 B + 0.044561 C \\ & + 1.62794 \cdot 10^{-3} AB - 1.71199 \cdot 10^{-5} AC + 0.027848 BC \\ & - 3.69989 \cdot 10^{-5} A^2 - 56.23451 B^2 - 1.59685 \cdot 10^{-4} C^2 \end{aligned} \quad (3)$$

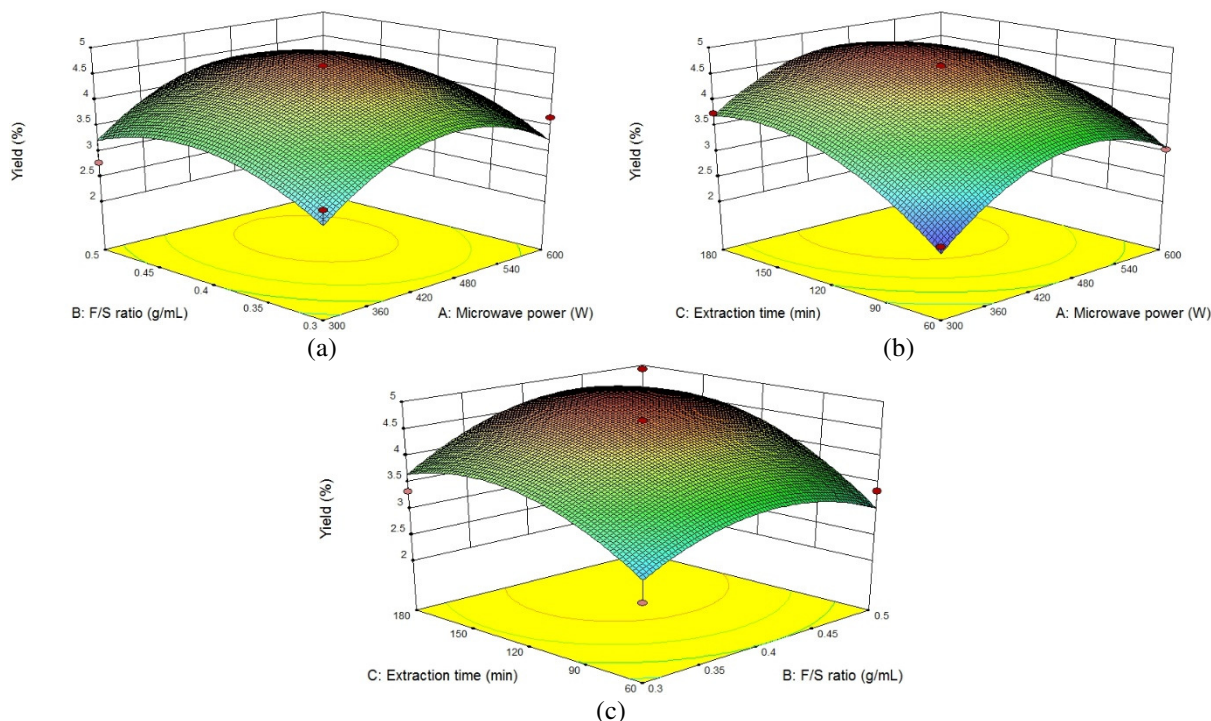


Fig.-2: Response surface showing effect of (a) microwave power and feed to solvent (F/S) ratio on the yield at constant extraction time (120 min); (b) microwave power and extraction time on the yield at constant feed to solvent (F/S) ratio (0.4 g/mL); (c) feed to solvent (F/S) ratio and extraction time on the yield at constant microwave power (450 W)

Experimental data generated in Table-2 in terms of actual values were substituted into Equation-3 and the predicted patchouli oil yield was obtained. Actual patchouli oil yield and the predicted patchouli oil yield are presented in Table-2; Comparison of these values indicates that the 2 sets of values are in close agreement. This suggests good reliability of the model as also evidenced from the statistical parameters of the model such as standard deviation of 0.40, R^2 of 0.9036 and F-value of 7.29. This shows fitness of the data for the model.

Numerical optimization method was used to predict optimum condition for the response using the Design-Expert version 9.0.4.1 (State-Ease Inc., Minneapolis, MN, USA). The microwave power of 467.517 W, feed to solvent ratio of 0.432 g/mL and extraction time of 152.122 min were obtained among the solutions for the optimum conditions for the yield. This condition gives a yield of 4.862%.

CONCLUSION

The optimization model was developed using response surface methodology technique for prediction of patchouli oil yield in microwave hydrodistillation of dried patchouli leaves. The model fits experimental data. The extraction time is the major process parameters found to significantly influence the patchouli oil yield. The conditions of optimum patchouli oil yield predicted were microwave power of 467.517 W, feed to solvent ratio of 0.432 g/mL and extraction time of 152.122 min, which gives patchouli oil yield of 4.862%.

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